

Study of Pumping Capacity of Pitched Blade Impellers

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A study was made of the pumping capacity of pitched blade impellers in a cylindrical pilot plant vessel with four standard radial baffles at the wall under a turbulent regime of flow. The pumping capacity was calculated from the radial profile of the axial flow, under the assumption of axial symmetry of the discharge flow. The mean velocity was measured using laser Doppler anemometry in a transparent vessel of diameter $T = 400$ mm, provided with a standard dished bottom. Three and six blade pitched blade impellers (the pitch angle varied within the interval $\alpha \in \langle 24^\circ; 45^\circ \rangle$) of impeller/vessel diameter ratio $D/T = 0.36$, as well as a three blade pitched blade impeller with folded blades of the same diameter, were tested. The calculated results were compared with the results of experiments mentioned in the literature, above all in cylindrical vessels with a flat bottom. Both arrangements of the agitated system were described by the impeller energetic efficiency, i.e., a criterion including in dimensionless form both the impeller energy consumption (impeller power input) and the impeller pumping effect (impeller pumping capacity). It follows from the results obtained with various geometrical configurations that the energetic efficiency of pitched blade impellers is significantly lower for configurations suitable for mixing solid-liquid suspensions (low impeller off bottom clearances) than for blending miscible liquids in mixing (higher impeller off bottom clearances).

Keywords: pitched blade impeller, impeller pumping capacity, turbulent flow, laser Doppler anemometer, impeller energetic efficiency.

1 Introduction

The pumping capacity of a pitched blade impeller (PBT) is defined [1] as the amount of liquid leaving the rotor region of the impeller, i.e., the cylindrical volume circumscribed by the rotating impeller blades, per unit time. This quantity is an important process characteristic of the PBT and plays an important role when calculating the blending or homogenization time of miscible liquids in mixing [2,3], in the design of continuous-flow stirred reactors [4] and in calculating the process characteristics of solid-liquid suspensions [5], i.e. the impeller frequency for just off bottom suspension.

The pumping capacity of a PBT can be measured by the indirect "flow follower" (indicating particle) method [1] and calculated from the measured mean time of liquid primary circulation, or calculated [3, 5, 6] from the known radial profile of the axial component of the mean velocity in the impeller discharge stream leaving the impeller rotor region by means of integration over the circular cross section of the impeller rotor region.

The pumping capacity of the PBT Q_p can be expressed in dimensionless form as the impeller flow rate number [1, 2]

$$N_{Q_p} = Q_p / n D^3, \quad (1)$$

where n is the frequency of the impeller revolution and D is its diameter. Quantity N_{Q_p} does not depend on the Reynolds number of the impeller when this quantity exceeds ten thousand [1, 3, 6]. For impeller power input P the Power number has been introduced

$$Po = P / \rho n^3 D^5, \quad (2)$$

where ρ is the density of the agitated liquid. This quantity is also independent of the impeller Reynolds number when it exceeds ten thousand. A combination of the dimensionless quantities N_{Q_p} and Po gives the so called hydraulic efficiency of the impeller [2, 7] defined as

$$E_p = \frac{N_{Q_p}^3}{Po} \left(\frac{D}{T} \right)^4, \quad (3)$$

where T is the diameter of the vessel.

The higher the quantity E_p , the greater the ability to convert impeller energy consumption into its pumping effect.

This study deals with an analysis of the pumping and energetic efficiency of various pitched blade impellers under two main geometrical conditions: conditions convenient for solid-liquid suspensions operations and conditions convenient for blending miscible liquids. The PBT pumping capacity will be calculated from the radial profile of the axial component of the mean velocity in the impeller discharge stream leaving the impeller rotor region. The velocity profile will be determined by laser Doppler anemometry.

2 Experimental

Experiments were carried out in a pilot plant cylindrical vessel with adished bottom [9] – see Fig. 1. The vessel had

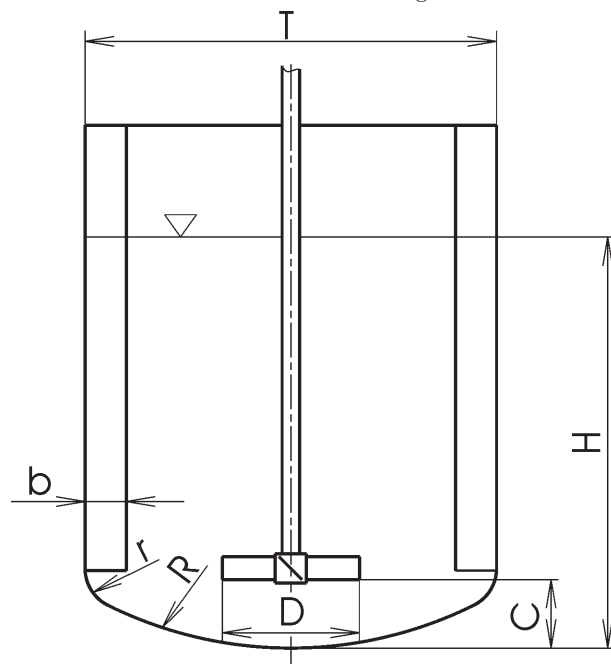


Fig. 1: Layout of test rig with dished bottom ($H/T = 0.36$, $C/D = 0.5$, $b/T = 0.1$, $R/T = 1$, $r/T = 0.1$)

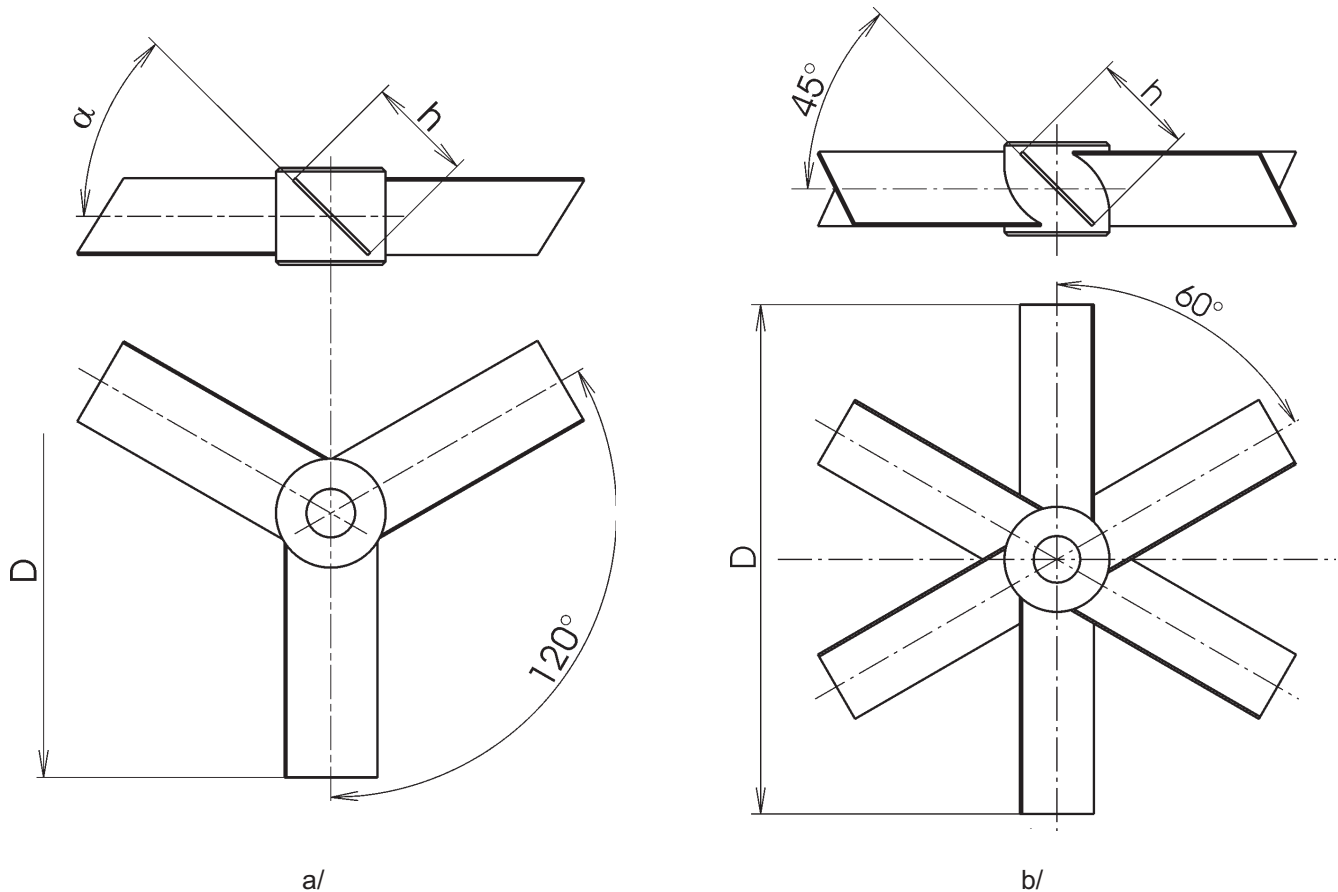


Fig. 2: Sketch of pitched blade impellers with three or six blades – Czech Standard CVS 691020 (a/ $n_B=3$: $\alpha=24^\circ, 35^\circ, 45^\circ$, b/ $n_B=6$: $\alpha=45^\circ$, $h/D=0.2$)

diameter $T=400$ mm and was equipped with four equally spaced radial baffles mounted at the wall. It was filled with water at a temperature of 20°C to a height of $H=T$. The frequency of revolution of the impeller was measured by means of a photoelectric cell with an accuracy ± 1 rev/min.

Figs. 2 and 3 show geometrical sketches of the pitched blade impellers used in this study. Two types of impellers were investigated: simple PBTs (see Fig. 2) and a PBT with folded blades (see Fig. 3). Both types of impellers had a

relative diameter $D/T=0.36$ and relative off bottom clearance $C/D=0.5$. The off bottom clearance was measured from the centre of the dished bottom to the lower edge of the impeller using a ruler, with a precision of ± 1 mm. The error in measuring the blade angle of the PBTs can be considered as $\pm 0.5^\circ$. All the PBTs rotated in such a way that they pumped liquid downwards towards the bottom.

The mean velocity field in the impeller discharge flow just below the impeller rotor region was measured with a laser Doppler anemometer (LDA). A DANTEC 55X two component modular series LDA and its associated BSA data processor, connected with a PC, was used for the experiments. The LDA was operated in a forward scatter mode (see Fig. 4). The laser (5-W Ar ion, manufactured by Spectra Physics,

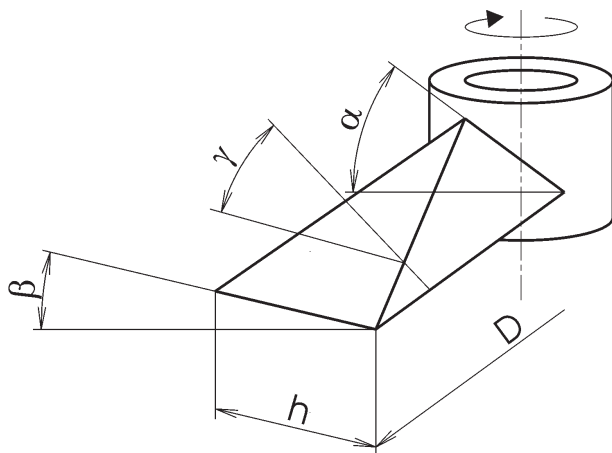


Fig. 3: Sketch of a pitched blade impeller with folded blades – Czech Standard CVS 691010 ($n_B=3$, $s/D=1.5$, $\alpha=67^\circ$, $\beta=25^\circ$, $\gamma=48^\circ$, $h/D=0.2$)

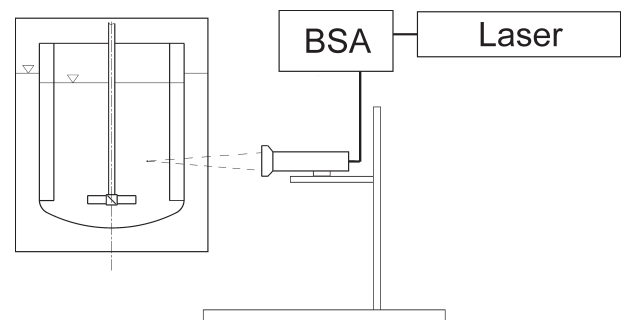


Fig. 4: Layout of a laser Doppler anemometer with forward scatter mode

USA) and optics were mounted on a bench which has a two-dimensional traversing mechanism. To identify the flow reversals correctly, a frequency shift was given to one of the beams by means of a Bragg cell with electronic down-mixing. Two components of the local velocity were measured simultaneously, with positioning accuracy ± 0.1 mm. The sample size was set at 20,000 items for each velocity measurement, and the mean time (averaged) value from all the samples was calculated.

3 Results and discussion

The impeller pumping capacity Q_p was calculated from the experimentally determined radial profiles of the axial component of the mean velocity in the impeller discharge stream leaving the impeller rotor region $w_{ax}=w_{ax}(r)$. The local value of the mean velocity corresponds to the ensemble average value over the circle of radius r determined by LDA. Assuming axial symmetry of the impeller discharge stream, the impeller pumping capacity can be calculated from the equation

$$Q_p = 2p \int_0^{D/2} \overline{w_{ax}}(r) dr. \quad (4)$$

Fig. 5 depicts the measured radial profiles of the axial components of the mean velocity in the impeller discharge flow related to the impeller tip speed

$$W_{ax} = \frac{\overline{w_{ax}}}{\pi D n}, \quad (5)$$

at various impeller frequencies of revolution. This figure provides quite a good illustration of the independence of the dimensionless quantity w_{ax} from the frequency of revolution of the impeller corresponding to the fully turbulent regime of agitated liquid. Dimensionless radial coordinate $2r/T$ defines the velocity profile in the axial discharge flow [1]. In the vicinity of the impeller hub ($2r/T \in \langle 0; 0.1 \rangle$) the liquid velocity amounts to a zero value, then it increases in the region of the

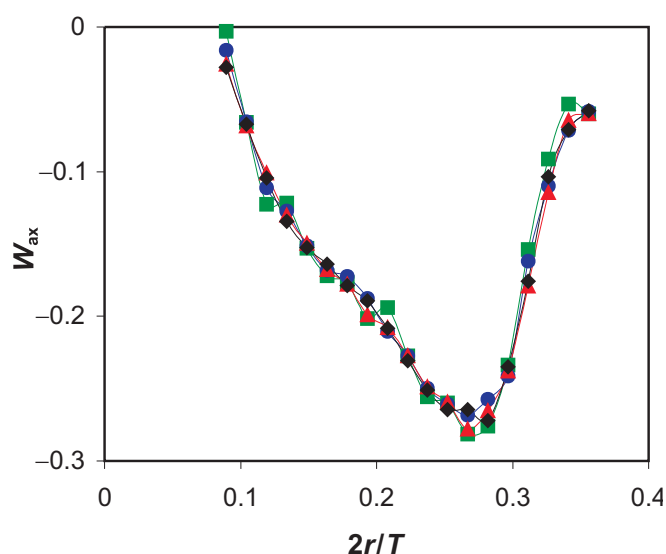


Fig. 5: Radial distribution of the axial component of the dimensionless mean velocity in a liquid leaving the rotor region of a pitched blade impeller – $n_B=3$, $\alpha=24^\circ$ (n [min⁻¹] – point: 162 – ■, 210 – ●, 261 – ▲, 310 – ◆)

Rankin forced vortex and, finally, it decreases in the region of the trailing vortices behind the impeller blades [1].

Table 1 consists of the above mentioned results of calculations for all the impellers tested (the value of criterion N_{Q_p} is the arithmetic mean value from the values of Q_p (or N_{Q_p}), calculated according to formulas (1) and (4) from the experimental velocity data) and further values of the Power number P_0 calculated from Eq. 2. The impeller power input was also determined experimentally by means of a strain gauge torque meter mounted on the impeller shaft. Finally, the value of the impeller hydraulic efficiency was calculated from Eq. (3) and was included in Table 1.

Table 1: Dimensionless pumping and energetic characteristics of pitched blade impellers in a baffled system with a dish bottom ($H/T=1$, $D/T=0.36$, $C/D=0.5$)

n_B	α	N_{Q_p}	P_0	E_p
[-]	[°]	[-]	[-]	[-]
3	24	0.41	0.37	0.00312
3	35	0.51	0.79	0.00282
3	45	0.56	1.27	0.00232
6	45	0.65	1.81	0.00255

Table 2 consists of the dimensionless pumping and energetic characteristics of PBTs in a baffled system with a flat

Table 2: Dimensionless pumping and energetic characteristics of pitched blade impellers in a baffled system with a flat bottom

I. Results of Wu and co-workers [5] ($H/T=1$, $D/T=0.41$, $C/D=0.815$)

n_B	α	N_{Q_p}	P_0	E_p
[-]	[°]	[-]	[-]	[-]
4	20	0.43	0.27	0.00832
4	25	0.53	0.37	0.01137
4	30	0.58	0.56	0.00951
4	35	0.65	0.73	0.01063
4	40	0.72	0.97	0.01087
4	45	0.76	1.22	0.1016
2	30	0.49	0.45	0.00739
3	30	0.54	0.53	0.00840
5	30	0.60	0.69	0.00847
6	30	0.61	0.72	0.00891

II. Results of Fořt and Medek [7] ($D/T=0.33$, $C/D=0.1$)

n_B	α	E_p	Note
[-]	[°]	[-]	
2–6	25–60	0.00742	Impeller with folded blades (see Fig. 3)
2–6	$s/D=1.0–1.25$	0.00864	

bottom found in the literature under conditions of higher off bottom impeller clearance than those set up in our study.

A combination of Eqs. (6) and (7) according to the definition of the hydraulic efficiency of the impellers (Eq. 3) gives for the squared configuration of the agitated system ($H/T = 1$)

$$E = n \left(\frac{C}{D} \right)^{0.244} \left(\frac{D}{T} \right)^{0.251} (\sin \alpha)^{0.468} \quad (8)$$

The flow rate criterion N_{Q_p} and the Power number Po were correlated in the literature on the basis of many experiments carried out for pitched blade impellers in a baffled flat bottomed cylindrical pilot plant agitated system (see Fig. 6) under a turbulent regime of an agitated liquid. Medek [7] published a correlation

$$Po = 1.507 n_B^{0.701} (C/D)^{-0.165} (T/D)^{-0.365} (H/T)^{0.140} (\sin \alpha)^{2.077} \quad (6)$$

while Medek and Fořt [1] published

$$N_{Q_p} = 0.745 n_B^{0.233} (C/D)^{0.254} (T/D)^{0.023} (H/T)^{0.251} (\sin \alpha)^{0.468}. \quad (7)$$

The intervals of the validity of the two correlations are as follows:

$$n_B \in \langle 2; 8 \rangle, C/D \in \langle 0.2; 1.0 \rangle, T/D \in \langle 2.45; 5.93 \rangle, H/T \in \langle 0.55; 1.0 \rangle, \alpha \in \langle 15^\circ; 60^\circ \rangle, 4 \text{ baffles } (b/T = 0.1), Re_M > 1.0 \cdot 10^4.$$

Taking the data of Kresta and Wood [6] and comparing it with correlation (7) we can write the relation

$$N_{Q_p} \sim (C/D)^{0.244}, D/T = 1/3, H/T = 1, C/D \in \langle 0.165; 0.875 \rangle. \quad (8)$$

The exponent at the geometrical simplex C/D mentioned in Eq. (8) following from the data of Kresta and Wood corresponds fairly well to the exponent at the same simplex in Eq. (7). Similarly, we can compare relation [5]

$$N_{Q_p} \sim n_B^{0.215}, D/T = 0.41, H/T = 1, C/D = 0.813, n_B \in \langle 2; 6 \rangle \quad (9)$$

with the corresponding relation within Eq. (7) and, again, the two exponents for the equivalent quantity (n_B) agree fairly well.

phenomenon is more apparent when the dished bottom of the cylindrical vessel is introduced.

List of Symbols

b	baffle width, m
C	off bottom impeller clearance, m
D	impeller diameter, m
E_p	impeller hydraulic efficiency
H	height of liquid from bottom of vessel, m
h	width of impeller blade, m
N_{Q_p}	flow rate number
n	impeller frequency of revolution, s^{-1}
n_B	number on impeller blades
P	impeller power input, W
P_o	power number
Q_p	impeller pumping capacity, $m^3 s^{-1}$
Re_M	Reynolds number
R	radius of dished bottom, r
r	radius of round corners of dished bottom, m
r	radius, m
s	pitch, m
T	vessel diameter, m
W_{ax}	dimensionless axial component of the liquid mean velocity
w_{ax}	axial component of the liquid mean velocity, $m s^{-1}$
α	pitch angle of blade, $^\circ$
β	pitch angle of blade, $^\circ$
γ	angle, $^\circ$
ρ	density of agitated liquid, $kg m^{-3}$

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