

Models for Non-isothermal Steady-State Diffusion in Porous Building Materials

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Two models for non-isothermal diffusion of water vapour in building materials have been developed and their numerical outputs compared with a standard isothermal approximation.

Keywords: Fick's laws, non-isothermal diffusion, partial pressure profile.

1 Introduction

The structure of most building materials of silicate origin consists of mutually interconnected microscopic pores. The diameters of the pores show wide dispersion in their values ranging from nanometers to millimeters. Since the mean free path of water vapour molecules at normal room conditions lies below 1 nm, almost all pores are open for vapour diffusion. However, this is not the only transport mechanism that enables moisture to enter a building material. At higher relative humidity (approx. above 50 %) intensive capillary condensation occurs on the surface of pores and the pores are subsequently filled with liquid water which can migrate into a material. Liquid transport in pores takes place both by surface diffusion and by capillary flow. However, the purpose of this paper is to deal with diffusion of the gas phase only, i.e., of water vapour, without the liquid transport. This simplification is commonly applied, e.g., within the Glaser condensation model [1], widely used in thermal building technology.

A common practice in thermal building technology is to calculate the vapour diffusion flux and pressure profile $p(x)$ inside building envelopes within an isothermal model, although the envelopes normally experience non-isother-

mal conditions throughout the year. The temperature of the medium within the building envelope is represented by a constant temperature in a given climate region, e.g., 19°C for Central Europe. Such an approximation has been shown to be very dangerous for thermal analysis of building envelopes [2]. It can be seen in some former papers [3, 4]

this procedure might provide satisfactory results for one-year assessment of envelopes, it is clear that the results for a shorter period can show severe deviations from the experimental data.

2 Non-isothermal diffusion

Let us suppose that the building envelope through which the diffusion flux goes is represented by a plain brick wall of thickness $d = 44$ cm. The wall separates a heated room with a usual environment (surface temperature and relative humidity: $T_1 = 293.15$ K, $\phi_1 = 60$ % RH) from an outdoor space ($T_2 = 255.15$ K, $\phi_2 = 84$ % RH). The atmospheric pressure of dry air is usually considered to be approximately the same on both sides ($p_a = 98066.5$ Pa – used in [4]). The atmospheric pressure p consists of partial pressures of water vapor p_w and dry air p_a

$$p = p_w + p_a, \quad p_w \ll p_a, \quad p \approx p_a. \quad (1)$$

Similar relations also hold for mass concentrations as well

$$c = c_w + c_a, \quad c_w \ll c_a, \quad c \approx c_a. \quad (2)$$

A reasonable choice [5] for the temperature profile $T(x)$ of a wall is the linear function

$$T(x) = T_1 - \frac{T_1 - T_2}{d} x, \quad (T_1 > T_2). \quad (3)$$

Fick's first law for non-isothermal diffusion assumes the following form [12]

$$q_w = y_w(q_w + q_a) - cD_{wa}(T)\nabla y_w, \quad y_w = \frac{c_w}{c} = \frac{c_w}{c_w + c_a} \quad (4)$$

where q_w and q_a are diffusion fluxes of water vapor and air, respectively, and $D_{wa}(T)$ is the temperature-dependent diffusivity. The diffusion flow should fulfil the condition of continuous flow

$$c \frac{\partial y_w}{\partial t} = \nabla q \quad (5)$$

which is Fick's second law. Assuming unidirectional steady-state diffusion ($\partial y_w / \partial t = 0$) along the x -axis and a negligibly small diffusion flow ($q_a \rightarrow 0$) of heavy air molecules ($N_2 + O_2 + \dots$) as compared with lighter H_2O molecules

(e.g., $D_{wa} \approx 10^{-10}$ m²s⁻¹ at 20°C and 1 atm)

$$D_{wa} = \frac{k}{\mu} T^n, \quad n = 1.81, \quad k = 8.9718 \times 10^{-10} \text{ m}^2 \text{ s}^{-1} \text{ K}^{-1.81} \quad (6)$$

$$\frac{\partial y_w}{\partial t} = 0 \Rightarrow \frac{\partial}{\partial x} \left(c \frac{\partial y_w}{\partial x} \right) = 0 \Rightarrow \frac{\partial}{\partial x} \left(\frac{c_w}{c} \frac{\partial c}{\partial x} \right) = 0 \quad (7)$$

with the boundary conditions

$$y_w(0) = y_{1w}, \quad y_w(d) = y_{2w}. \quad (8)$$

Following the work of Schirmer [4] and Krischer [6] the diffusivity of water vapor in the air pores of a material can be expressed as the function of temperature

$$D = \frac{k}{\mu} T^n, \quad n = 1.81, \quad k = 8.9718 \times 10^{-10} \text{ m}^2 \text{ s}^{-1} \text{ K}^{-1.81} \quad (9)$$

where μ is the 'diffusion resistance factor' – a purely material constant corresponding to the wall material. According to the gas law, mass concentration c is a function of pressure and temperature

$$c = \frac{p}{R_a T} \approx \frac{p_a}{R_a T}, \quad R_a = \frac{R}{M_a} \approx 297 \text{ J kg}^{-1} \text{ K}^{-1}, \quad (10)$$

$$R = 8.31 \text{ J mol}^{-1} \text{ K}^{-1}.$$

From Eqs. (3) – (10) it follows

$$\frac{p_a k}{R_a \mu} \int_{y_{1w}}^{y_w(x)} \frac{dy_w}{1 - y_{1w}(1+r)} = -q_w \int_0^x \left[T_1 + \frac{T_1 - T_2}{d} x \right]^{1-n} dx. \quad (11)$$

Inserting the second boundary condition (8) into (11) we obtain the diffusion flux

$$q_w = \frac{p_a k(2-n)}{R_a d \mu (1+r)} \cdot \frac{T_1 - T_2}{T_1^{2-n} - T_2^{2-n}} \cdot \ln \left[\frac{1 - y_{2w}(1+r)}{1 - y_{1w}(1+r)} \right], \quad (12)$$

$n = 1.81$

which, together with (11), gives the vapor profile $y_w(x)$

$$y_w(x) = \frac{1}{1+r} \left\{ 1 - [1 - y_{1w}(1+r)] \cdot \frac{T_1^{2-n} - \left(T_1 - \frac{T_1 - T_2}{d} x \right)^{2-n}}{T_1^{2-n} - T_2^{2-n}} \cdot \left[\frac{1 - y_{2w}(1+r)}{1 - y_{1w}(1+r)} \right]^{-\frac{2-n}{n}} \right\}, \quad n = 1.81 \quad (13)$$

Taking into account the *diffusion through an immobilized air layer* (**DIAL** model), i.e., $q_a \rightarrow 0$ ($r \rightarrow 0$), relations (12), (13) can be simplified

$$q_w^* = \frac{0.19 p_a k}{R_a d \mu} \frac{T_1 - T_2}{T_1^{0.19} - T_2^{0.19}} \cdot \ln \left[\frac{1 - y_{2w}}{1 - y_{1w}} \right], \quad (14)$$

$$y_w^*(x) = \left\{ 1 - (1 - y_{1w}) \cdot \left[\frac{1 - y_{2w}}{1 - y_{1w}} \right] \frac{T_1^{0.19} - \left(T_1 - \frac{T_1 - T_2}{d} x \right)^{0.19}}{T_1^{0.19} - T_2^{0.19}} \right\}. \quad (15)$$

Relation (14) may be formally rewritten as follows

$$q_w^* = \frac{\ln \left[\frac{1 - y_{2w}}{1 - y_{1w}} \right]}{R_{eff}^*}, \quad R_{eff}^* = \frac{d}{D_{eff}^*} \text{ [kg}^{-1} \text{m}^2 \text{s}], \quad (16)$$

where

$$D_{eff}^* = \frac{0.19 k p_a}{\mu R_a} \frac{T_1 - T_2}{T_1^{2-n} - T_2^{2-n}} = \frac{5.629 \times 10^{-8}}{\mu} \cdot \frac{T_1 - T_2}{T_1^{0.19} - T_2^{0.19}} \text{ [kg m}^{-1} \text{s}^{-1}].$$

Since $y_{1w} \ll 1$ and $y_{2w} \ll 1$, further simplification can be performed

$$\ln \left[\frac{1 - y_{2w}}{1 - y_{1w}} \right] \approx y_{1w} - y_{2w}, \quad q_w^* \approx \frac{y_{1w} - y_{2w}}{R_{eff}^*} \text{ [kg m}^{-2} \text{s}^{-1}]. \quad (17)$$

3 DRAL model

Relations (14) – (17) hold within the framework of the **DIAL** approximation, when the air layer embedded in a porous material is only slightly perturbed by the diffusion of water vapor molecules that possess smaller mass and much lower concentration than those of air. It seems to be natural that not only the pressure of dry air remains constant but also the concentrations of dry and wet air vary only slightly across the wall. This can be nicely illustrated when the concentration ratios are calculated for a particular case, e.g., for the internal and external conditions defined at the beginning of the previous Section

$$\begin{aligned} c_w^{\text{inner}} / c_w^{\text{outer}} &\approx 16.23, \\ c_a^{\text{inner}} / c_a^{\text{outer}} &= 0.870, \\ c^{\text{inner}} / c^{\text{outer}} &= 0.883 \end{aligned} \quad (18)$$

From (18) it can be seen that the variations of air concentrations c_a , c across the wall are negligibly small and, thus, the profiles $c_a(x)$, $c(x)$ may be considered as approximately horizontal, i.e., constant for common climatic conditions. This does not hold at all for water vapor whose concentration varies considerably and, thus, its profile shows clear functional dependence on x

$$\begin{aligned} c_w &= f(x), \quad c_a \approx \text{const.}, \\ c &\approx \text{const.}, \quad c_w(x) \ll c_a. \end{aligned} \quad (19)$$

If these relations are included into Fick's Eq.(6), we can obtain a more simplified transport equation

$$q_d = -D_{wa}(T) \frac{dc_w(T, p_w)}{dx}, \quad 1 - y_w \approx 1, \quad r \approx 0, \quad c \approx \text{const.} \quad (20)$$

An analogous transport equation holds for non-isothermal diffusion of a gas in a solid *compact* body, so present approximation might be termed as Diffusion through a 'Rigid' Air Layer (**DRAL** model). At first sight this approximation might seem rather unrealistic, but the final account of all physical factors and their *approximate behavior* leads to such a conclusion. Eq. (20) is quite analogous to those presented in technical literature for cases when the total concentration is constant (see e.g. Eq. 16.2–3 in [7]). The assumption $c = \text{const.}$ does not necessarily mean the condition for the isothermal state. Nearly constant total concentration c can be expected not only with non-isothermal diffusion of a gas in a solid *compact* body which does not contain any air pores but also in solid materials containing *closed* pores (cavities) filled with air. The diffusion flux in such materials goes either through the airless solid structures whose concentration (density) is almost unaffected by temperature and through voids with a constant air content (constant concentration), provided the walls of the voids are hardly penetrable for heavy air molecules in contrast to lighter water molecules. Foam building materials such as foam polyethylene approach this type of material. It seems probable that the DRAL model might be more applicable to such materials. However, it is necessary to stress that if a strong non-isothermal state causes essential variations in the total concentration profile, i.e., $c = f(x)$, the DRAL model will fail to determine a realistic diffusion flux. Briefly, the transport equation (20) should enable the diffusion flux of water

vapor in various materials to be approximated only under usual climatic conditions, since such conditions represent a weakly non-isothermal state which does not essentially disturb the total concentration profile. Nevertheless, for a highly non-isothermal state, the DRAL model can yield correct results only with quite special materials. Numerical comparison of the results obtained by various models is presented in Section 5.

Let us continue determining the solution of differential equation (20). First, it is necessary to specify the complete set of Fick's equations within the DRAL approximation

$$q_w = -\frac{D}{R_w} \frac{d}{dx} \left(\frac{p_w(x)}{T(x)} \right), \quad c_w = \frac{p_w}{R_w T}, \quad R_w = 462 \text{ J kg}^{-1} \text{ K}^{-1}, \quad (21)$$

$$\frac{d}{dx} \left[\frac{k}{\mu R_w} T^n(x) \frac{d}{dx} \left(\frac{p_w(x)}{T(x)} \right) \right] = 0, \quad n = 1.81 \quad (22)$$

and the boundary conditions belonging to a non-isothermal wall of thickness d

$$\frac{p_w(0)}{T(0)} = \frac{p_{1w}}{T_1}, \quad \frac{p_w(d)}{T(d)} = \frac{p_{2w}}{T_2}. \quad (23)$$

Since the non-linear temperature profile $T(x)$ appears in common walls only under special conditions [10], a linear profile is assumed here as well

$$T(x) = T_1 - \frac{T_1 - T_2}{d} x = a - bx. \quad (24)$$

Inserting (24) into Fick's equations (21), (22) and taking into account the first boundary condition (23), the corresponding solution can be found

$$\frac{k}{\mu R_w} (a - bx)^n \frac{d}{dx} \left(\frac{p_w}{T} \right) = -q_d = \text{const.}, \quad (25)$$

$$\frac{p_w(x)/T(x)}{\frac{p_{1w}}{T_1}} = \int_0^x \frac{q_d R_w \mu}{k} (a - bx)^{-n} dx, \quad (26)$$

$$q_w = \frac{\left(\frac{p_{1w}}{T_1} - \frac{p_{2w}}{T_2} \right) k b (1-n)}{\mu R_w [a^{1-n} - (a - bd)^{1-n}]}. \quad (27)$$

Inserting the second boundary condition (23) into (27), we can express the steady-state diffusion flux q_w

$$q_w = \frac{\left(\frac{p_{1w}}{T_1} - \frac{p_w(x)}{T(x)} \right) k b (1-n)}{\mu R_w [a^{1-n} - (a - bd)^{1-n}]} \quad (28)$$

which goes through a non-isothermal wall with a linear temperature profile (24). The symbols a , b in (28) can be specified using (24)

$$q_w = \frac{k(1-n)}{\mu R_w d} \frac{\left(\frac{p_{1w}}{T_1} - \frac{p_{2w}}{T_2} \right) (T_1 - T_2)}{T_1^{1-n} - T_2^{1-n}}, \quad n = 1.81. \quad (29)$$

Relation (29) can be rearranged and the effective diffusion coefficient D_{eff} and effective activation D_{eff} may be introduced

$$q_w = \frac{c_{1w} - c_{2w}}{R_{\text{eff}}} [\text{kg m}^{-2} \text{s}^{-1}],$$

$$R_{\text{eff}} = \frac{d_w}{D_{\text{eff}}} [\text{m}^2 \text{s}], \quad (30)$$

$$D_{\text{eff}} = \frac{k(n-1)(T_1 - T_2)}{\mu (T_2^{1-n} - T_1^{1-n})} [\text{m}^2 \text{s}^{-1}]$$

where

$$c_{1w} = \frac{p_{1w}}{R_w T_1} [\text{kg m}^{-3}], \quad c_{2w} = \frac{p_{2w}}{R_w T_2} [\text{kg m}^{-3}].$$

By means of relations (30) the non-isothermal diffusion flux q_w expressed within the DRAL approximation can be easily calculated.

For completeness, the partial pressure profile $p_w(x)$ inside the wall should be presented. Functions $p_w(x)$ and $c_w(x)$ are given by Eqs. (27) and (28)

$$p_w(x) = \left(T_1 - \frac{T_1 - T_2}{d} x \right) \cdot \left[\frac{\frac{p_{1w}}{T_1} - \left(\frac{p_{1w}}{T_1} - \frac{p_{2w}}{T_2} \right) \frac{T_1^{1-n} - \left(T_1 - \frac{T_1 - T_2}{d} x \right)^{1-n}}{T_1^{1-n} - T_2^{1-n}}}{T_1^{1-n} - T_2^{1-n}} \right], \quad (31)$$

$$c_w(x) = \frac{p_{1w}}{R_w T_1} - \left(\frac{p_{1w}}{R_w T_1} - \frac{p_{2w}}{R_w T_2} \right) \frac{T_1^{1-n} - \left(T_1 - \frac{T_1 - T_2}{d} x \right)^{1-n}}{T_1^{1-n} - T_2^{1-n}}. \quad (32)$$

For $n = 1.81$ the profiles $p_w(x)$ and $c_w(x)$ will read

$$p_w(x) = \left(T_1 - \frac{T_1 - T_2}{d} x \right) \cdot \left[\frac{\frac{p_{1w}}{T_1} - \left(\frac{p_{1w}}{T_1} - \frac{p_{2w}}{T_2} \right) \frac{T_1^{-0.81} - \left(T_1 - \frac{T_1 - T_2}{d} x \right)^{-0.81}}{T_1^{-0.81} - T_2^{-0.81}}}{T_1^{-0.81} - T_2^{-0.81}} \right], \quad (33)$$

$$c_w(x) = c_{1w} - (c_{1w} - c_{2w}) \frac{T_1^{-0.81} - \left(T_1 - \frac{T_1 - T_2}{d} x \right)^{-0.81}}{T_1^{-0.81} - T_2^{-0.81}}. \quad (34)$$

At first sight it is obvious that the $p_w(x)$ and $c_w(x)$ profiles are not linear. Nevertheless, for usual temperature and partial pressure differences between outdoor and indoor spaces in the Central European climatic region the graphs of $p_w(x)$ and $c_w(x)$ will closely follow linear behaviour, as can be easily verified.

4 IM-TDR and IM-TIR models

Glaser's standard condensation model [11] is based on isothermal diffusion, i.e. the temperature of a wall is considered to be a constant T_{int} and equal to the mean value of the surface temperatures

$$T_{\text{int}} = \frac{T_1 + T_2}{2}. \quad (35)$$

Fick's equations for diffusion in an isothermal state can be obtained from (21) and (22) after inserting $T = T_{\text{int}}$

$$q_d = -\frac{D}{R_w T_m} \cdot \frac{dp_w}{dx}, \quad \frac{dq_d}{dx} = 0. \quad (36)$$

where

$$D = \frac{k}{\mu} T_m^n, \quad n = 1.81.$$

Using the following boundary conditions

$$p_w(0) = p_{1w}, \quad p_w(d) = p_{2w} \quad (37)$$

the solution of (36) can be found easily

$$q_d = \frac{p_{1w} - p_{2w}}{R_d}, \quad R_d = \frac{\mu d}{\delta}, \quad \delta = \frac{k T_m^{n-1}}{R_w}, \quad n = 1.81 \quad (38)$$

$$p(x) = p_{1w} - \frac{p_{1w} - p_{2w}}{d} x. \quad (39)$$

As can be seen, the pressure profile $p(x)$ is a linear function of x in contrast to non-isothermal profiles (15) and (34), which are non-linear. In spite of the fact that Fick's Eqs. (36) hold exactly for isothermal structures only, i.e., for a constant temperature, the thermal resistance R_d is actually temperature dependent $R_d(T_m)$. Such a model may be termed as an 'isothermal model with temperature dependent resistance', i.e., IM-TDR.

Nevertheless, in civil engineering practice Fick's isothermal equations are combined with thermal resistance that is not temperature dependent, because the average temperature is fixed in the one-dimensional case, i.e., $T_m = 25^\circ\text{C}$ or regardless of the actual value T_m of a particular structure. Such a model may be called an 'isothermal model with temperature independent resistance', i.e., IM-TIR.

TABLE 1. Diffusion fluxes through the brick wall (wall thickness $d = 0.24\text{ m}$, $R_w = 0.55\text{ m}^2\text{K/W}$, $p_{1w} = 1402.2\text{ Pa}$, $p_{2w} = 1402.2\text{ Pa}$) and increasing temperature (for $R_d = 0.001\text{ m}^2\text{K/W}$)

Quantity	25°C (20°C)	50°C (30°C)	75°C (50°C)	100°C (70°C)	175.18 K (500 °C)	275.18 K (1000 °C)	5275.18 K (5000 °C)
p_w [Pa]	1402.2	1402.2	1402.2	1402.2	1402.2	1402.2	1402.2
$c_w \times 10^3$ [kg m ⁻³]	10.350	10.000	9.392	8.1340	3.9300	2.3800	5.7600
$\gamma_w \times 10^3$	9.1	9.1	9.1	9.1	9.1	9.1	9.1
IM-TIR $R_d \times 10^{-9}$ [m s ⁻¹]	20.956	20.956	20.956	20.956	20.956	20.956	20.956
IM-TDR $R_d \times 10^{-9}$ [m s ⁻¹]	21.61	21.61	21.29	19.35	12.98	9.42	3.32
DIAL $R_{\text{eff}}^* \times 10^{-4}$ [kg m ⁻¹ s ⁻¹]	14.18	13.98	13.61	12.8	9.13	7.07	3.13
DRAL $R_{\text{eff}} \times 10^{-4}$ [m ² s ⁻¹]	17.13	16.62	15.68	13.75	7.00	4.38	1.15
IM-TIR $q \times 10^8$ [kg m ⁻² s ⁻¹]	6.19	6.19	6.19	6.19	6.19	6.19	6.19
IM-TDR $q \times 10^8$ [kg m ⁻² s ⁻¹]	6.00	6.00	6.10	6.70	10.00	13.77	39.07
DIAL $q \times 10^8$ [kg m ⁻² s ⁻¹]	5.93	6.02	6.18	6.57	9.21	11.9	26.87
DRAL $q \times 10^8$ [kg m ⁻² s ⁻¹]	5.52	5.48	5.42	5.27	4.34	3.40	-2.83

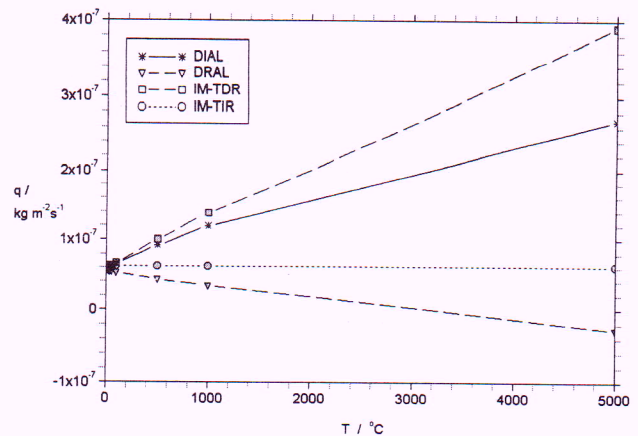


Fig. 1: Diffusion fluxes in dependence on temperature

5 Results and conclusions

In order to analyse the behaviour of all the models discussed, their results for the structure given at the beginning of Chapter 2 are presented in Fig. 1 and Table 1. The calculations were done for a brick wall with a thickness of 0.24 m, a thermal resistance of 0.55 m²K/W, and a constant pressure of water vapour removed from the wall. The external temperature was increased, increasing, i.e., the external relative humidity was decreasing. Such a condition may be found in the case of increasing temperature, i.e., $T = T_0 + T_1 \sin(\omega t)$, on the external surface of the wall.

Table 1 and Fig. 1 show that at 'small' temperature differences ($\Delta T < 40$ K) the heat fluxes of all four models differ only by a few percent and, thus, under such 'quasi-isothermal' conditions all the models give nearly identical results. Since the temperature difference ΔT in the Central European climatic region does not usually exceed fifty Kelvin during a year, all the models seem to be applicable within civil engineering practice.

Nevertheless, if strongly non-isothermal conditions are established ($\Delta T > 40$ K), it is necessary to distinguish carefully between computational models. While the IM, TIP and PM are most applicable in all meteorologic conditions, the applicability of the remaining three models will depend on the material properties. For instance, while the Fick model is applicable with air (but is still not reliable in building materials as demonstrated by the counterexamples), the model can be used for PVC and PC-PC. The use of which should be given, primarily in practical calculations. The applicability of the third model under strongly non-isothermal conditions can be determined by comparing a numerical result calculation results to be calculated, which is suitable only for qualitative materials.

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